
Published by: Royal Society of Chemistry

URL: http://dx.doi.org/10.1039/C6SM00767H <http://dx.doi.org/10.1039/C6SM00767H>

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Collective and convective effects compete in patterns of dissolving surface droplets

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The effect of neighboring droplets on the dissolution of a sessile droplet, i.e. collective effects, are investigated both experimentally and numerically. On the experimental side small 20 nl approximately mono-disperse surface droplets arranged in an ordered pattern were dissolved and their size evolution is studied optically. The droplet dissolution time was studied for various droplet patterns. On the numerical side, Lattice-Boltzmann simulations were performed. Both simulations and experiments show that the dissolution time of a droplet placed in the center of a pattern can increase with as much as 60% as compared to a single, isolated droplet, due to the shielding effect of the neighboring droplets. However, the experiments also show that neighboring droplets enhance the buoyancy driven convective flow of the bulk, increasing the mass exchange and counteracting collective effects. We show that this enhanced convection can reduce the dissolution time of droplets at the edges of the pattern to values below that of a single, isolated droplet.

1 Introduction

The evaporation or dissolution of a single surface droplet is a well-studied topic due to its high importance in various applications, for example in the field of coating, and the deposition of particles. Even more relevant but far less studied is the evaporation or dissolution of surface droplets surrounded by other droplets. This situation for example occurs whenever a spray is applied to a surface, or in inkjet printing. The presence of neighboring droplets makes the analytical approach more challenging as compared to a single droplet, and in general no analytical solution for the collective dissolution problem (on which we will focus here) exists. The addition of neighboring droplets, like in the pattern sketched in Fig. 1, is expected to change the concentration gradient by saturating the water in between the droplets, which in turn leads to a decrease in the mass loss rate. This change in concentration gradient, caused by the presence of the neighboring droplets, explains the observed increased droplet dissolution time.

In this paper, we further investigate the collective effect in patterns of dissolving surface droplets. A diffuse interface numerical scheme is introduced and applied to simulate this system, and the numerical results are compared to experiments. Simulations and experiments on single droplets, finite, and infinite patterns are conducted. In particular, we will discuss the competition between on the one hand the slowed down dissolution due to the enhanced surrounding concentration thanks to the neighboring droplets and the resulting slower diffusion, and on the other hand enhanced convection due to collective convective effects.

2 Methods

2.1 Experimental procedure

A dissolving sessile droplet of long-chain alcohols in water is a versatile system to study various aspects of the dissolution process. In the current work, 1-heptanol (Sigma-Aldrich, ≥98% purity) is used: a long-chain alcohol with an oily appearance, which has a saturation solubility $c_s = 1.67 \text{ g L}^{-1}$ in water, a diffusion constant $D = 0.8 \times 10^{-9} \text{ m}^2 \text{s}^{-1}$, and a density $\rho_d = 819 \text{ kg m}^{-3}$.

$2 \times 2 \text{ cm}^2$ pieces of silicon wafers (P/Boron/(100), Oxmetic), hydrophobized with PFDTDS (1H,1H,2H,2H-Perfluorodecylmethoxysilane 97%, ABCR GmbH, Karlsruhe Germany) were used as substrates. These substrates were cleaned by sonication in acetone, and dried under a stream of nitrogen, prior to the experiment. The substrate was then placed at the bottom of a $5 \times 5 \times 5 \text{ cm}^3$ glass tank, as sketched in Fig. 2. With the substrate in place, the cell was filled with 100 mL...
water, obtained from a millipore machine (Reference A+ system, Merck Millipore, at 18.2 MΩ cm). Subsequently, a glass-teflon syringe fitted with a thin needle (210 µm outer diameter) and connected to a motorized syringe pump, was put into the water. 20 nL ±4 nL droplets of the 1-heptanol were dispensed through the needle of the syringe and gently placed on the substrate. A motorized, computer controlled X-Y stage (Thorlabs) moved the cell and substrate with respect to the needle, and droplets were placed one by one to form patterns of \( n = 5, 19, 41, \) or 127 droplets, see for example Figs 3A-D. Droplets were placed in a hexagonal arrangement, as sketched in Fig. 1, with the exception of the outermost droplets in the largest pattern. All droplets in the experiments dissolved in the stick-jump mode \(^3, ^5, ^6\), causing the contact angle \( \theta \) of the droplet to vary between 65° and 70°. The time to create the largest pattern (127 droplets) was \( \approx 15 \) minutes, which should be compared to the total dissolution time of \( > 2.5 \) hours. The relatively large volume of water in the tank ensured that even after complete dissolution of the largest pattern, the bulk saturation level was \( \approx 0.02c_s \).

A collimated light emitting diode light source (Thorlabs, \( \lambda = 625 \) nm) produced a beam parallel to the substrate and projected the side view image of the center droplet in the pattern onto a CCD camera (Pixelfly USB, PCO Germany) fitted with a long working distance microscope. Since other droplets would obscure the view of the center droplet, only this droplet was placed in the center row. The white arrow in Fig. 3 indicates the center droplet, and the direction of view. Simultaneous measurements of the outermost droplets were unfortunately impossible, as their side view was obscured by the surrounding droplets, prohibiting the accurate contact angle determination required for volumetric measurements. The images obtained were post-processed in Matlab to extract the profile with sub-pixel accuracy\(^11\). Other experiments were carried out as well to provide a top view of the droplet pattern. To this purpose, a droplet pattern was deposited in the usual way after which the tank was placed under a Leica DM2500H microscope, operated in the incident light mode, using a \( 5 \times \) magnification objective.

Fig. 1 (color online) Schematic drawing of a pattern of surface droplets with footprint diameter \( L \) and contact angle \( \theta \), placed in a hexagonal pattern with center-to-center distances \( d \).

Fig. 2 (color online) Sketch (not to scale) of the experimental setup, showing the glass tank with the substrate placed under water. The syringe is connected to a syringe pump (not drawn) to dispense droplets of 1-heptanol. Using the X-Y translation stage, the tank is moved with respect to the syringe. A LED illuminates the middle droplet of the pattern, and projects the side view image of this droplet onto a long-distance microscope and CCD-camera.

Fig. 3 (color online) A-D: Top view photographs of the water-immersed silicon substrate with the droplet patterns. The photographs show patterns with 5 (A), 19 (B), 41 (C), and 127 (D) 20 nL sized droplets of 1-heptanol. Panel E is a schematic side view of the numerical set-up showing the shell (E1), side (E2), top (E3) boundary condition used to simulate a single drop, multiple drops and an infinite array of drops respectively. The dashed lines in E indicate the surfaces, where the chemical potential is fixed at a non-equilibrium value to drive dissolution. The wavy dashed lines in Fig. (E3) represent periodic boundary conditions.
2.2 Numerical procedure

We performed three-dimensional simulations using a hydrodynamics model based on the Navier-Stokes equations and the Cahn-Hilliard model into which we have implemented evaporation following ref. 12. The droplet-bulk system is considered as a binary liquid and by setting the chemical potential of the model at a value away from equilibrium, one phase is favored over the other. This physically corresponds to the situation that dissolution takes place if the solute concentration is lower than its saturation value (which is the equilibrium value). Three-dimensional surface droplets were simulated. For numerical optimization reasons we adopted a droplet contact angle of $\theta = 90^\circ$ and the following boundary conditions (see Fig. 3E):

1. For a single droplet, the chemical potential is fixed on a hemispherical shell surrounding the drop (referred to in the following as "shell BC");

2. For a finite pattern of droplets, the chemical potential is fixed at the top and the sides of the computational domain ("side BC");

3. For an infinite pattern of droplets, the chemical potential is fixed at a plane at the top of the computational domain and periodic boundary conditions are applied at the sides of it ("top BC").

More detailed information on the numerical procedure is provided in the appendix.

3 Results

3.1 Single droplet

To provide a simple test case and a basis to compare further measurements, we start with the dissolution of a single surface droplet, which has been well described in the context of the analogous processes of dissolving bubbles or evaporating droplets. In the case of steady-state, diffusion-limited dissolution, the dissolution rate of a droplet is given by\(^4,13-15\),

$$\frac{dV}{dt} = -\frac{\pi LD(c_s - c_o)}{2\rho_d} f(\theta),$$

where,

$$f(\theta) = \frac{\sin \theta}{1 + \cos \theta} + 4 \int_0^{\infty} \frac{1 + \cosh 2\theta e}{\sinh 2\pi e} \tanh[(\pi - \theta) e] de$$

is a geometrical factor to describe the effect of the droplet contact angle and the impermeable substrate. By inserting the values for a 1-heptanol droplet with initial volume $V_0 = 20$ nL, and numerical integration of Eq. (1), we obtain the black dashed line in Fig. 4 which represents the droplet volume as function of the time to dissolution $\tau - \tau$, where $\tau$ is the dissolution time: the time needed to completely dissolve the droplet.

Comparison of the experiments on single droplets of different initial volumes (plotted as the colored solid lines in Fig. 4) to the diffusion-limited model of a single droplet reveals a considerable discrepancy: the experiments are characterized by a higher rate of mass loss and therefore shorter dissolution time $\tau$ for a given initial volume. It has been shown\(^7\) that the increased mass transport is caused by a convective contribution to the dissolution process, driven by solute-induced density gradients in the bulk.

The experimental results from Fig. 4 will be used in the next section, as they allow us to account for the variation in the initial droplet volumes: Despite the fact that great care is taken to create equally sized droplets, small differences in the initial droplet volume cannot be avoided. To allow for easy comparison between experiments with slight variations in the initial droplet volume, we correct for these deviations and compare the droplet volume to the desired initial volume of the droplets in the experiments (20 nL), namely by correcting the droplet volume $V$ in each experiment according to

$$\tilde{V} = \frac{V}{V_0} \times 20 \text{ nL},$$

where $\tilde{V}$ is the corrected droplet volume (in nL), and $V$ and $V_0$ are the volume and the initial volume of the droplet, respectively. The differences in the initial droplet volumes (even though only a few nL) significantly affect the total droplet dissolution time, thus obscuring the possible influence of collective effects. Therefore we must also correct the (dissolution) time based on the initial volume, which in diffusive problems is usually achieved by scaling with the appropriate time scale, namely the diffusive time scale $\tau_4 = R_0^2 p / (\Delta c D)$, where $R_0$ is the initial droplet radius, and $\Delta c = c_a - c_m$. Scaling the time in such a way allows to compare purely diffusive droplet dissolution behavior, independent of the initial droplet size or the material\(^5,15\). Unfortunately, the diffusive time scale $\tau_4$ cannot be used in the current system as the mass transport is not purely diffusive. On the other hand, purely convective dissolution with the associated convective time scale\(^7\)

$$\tau_c = \frac{4}{5a} \left( \frac{V p R_0^4}{\beta g D} \right)^{1/4},$$

where $\beta$ is the bulk expansion coefficient, $g$ the acceleration of gravity, and $a$ a prefactor of order 1. Eq. (4) was shown to hold when the Rayleigh number

$$Ra = \frac{g \beta \Delta c R^3}{\nu D} > 12.$$  

The Rayleigh number expresses the ratio of the buoyant force to the damping force, and for the current 1-heptanol droplets with volumes $\leq 20$ nL, we find $0.5 < Ra < 35$. This indicates droplet dissolution with contributions to mass transport from both convection and diffusion. This does neither allow for the use of the purely convective model, nor the purely diffusive model. Instead, both diffusion and convection play a role.

Therefore to proceed we exploit the single-droplet experiments to give an empirical relation between the initial volume of a single droplet and its dissolution time $\tau_{\text{single}}(V_0)$. Using this relation, we correct time in each experiment according to

$$\hat{t} = \frac{t}{\tau_{\text{single}}(V_0)} \times 9100 \text{ s},$$

where $\hat{t}$ is the corrected time (in seconds), and $\tau_{\text{single}}(V_0)$ is...
Fig. 4 (color online) Volume of single dissolving droplets as function of time until dissolution \( t - \tau \). The black dashed line represents the expected diffusion-limited dissolution of a 20 nL 1-heptanol droplet (Eq. 1), to which the (purely diffusive) simulations (plotted as the open red diamonds) are compared. The experiments on individual droplets with of 1-heptanol and various initial volumes (solid lines of different colors) reveal an increased dissolution rate, due to a convective contribution to the dissolution. We shift the x-axis by the droplet life time \( t \) to overlap the individual measurements for comparison. The black arrows illustrate how the experiments can be used to find an empirical relation between the droplets initial volume and its dissolution time.

The use of a time scale in seconds, rather than a dimensionless time is preferred as it emphasizes that the simulations and experiments are subject to different physical processes: purely diffusive dissolution in the simulations versus a combination of diffusive and convective dissolution in the experiments. Therefore this comparison must be interpreted as qualitative, and not quantitative. The absence of convection in the simulations is mainly due to the fact that the two phases have equal densities, so no buoyancy is present. Currently, steps are being taken to also incorporate convection into the simulations, which opens the way to achieving quantitative agreement between the simulations and the experiments.

3.2 Droplet patterns: shielding mechanism

It has been proposed \(^4\) that the enhanced dissolution time for collective droplets is caused by a larger solute concentration in the (liquid) environment in between the droplets, due to their dissolving neighbors, thus reducing the concentration gradient and thus the mass transport. We confirm this by simulating a pattern with \( n = 5 \) droplets, and measuring the concentration along a diagonal cross-section through this pattern as shown in Figs. 5A and 5B. The solid colored lines, shown in panel A, represent five iso-concentration lines measured at \( t_1 = 1900 \) s along the cross-
Fig. 5 (color online) A) The iso-concentration profiles (colored lines, measured at $t_1 = 1900$ s) show how the concentration in between the droplets is increased due to the neighboring droplets. The profile is measured diagonally through a pattern with $n = 5$ droplets, as indicated by the dashed line in panel B. The (dashed) contours of the droplets correspond to times $t_1 = 1900$ s (outermost contours), $t_2 = 8500$ s, and $t_3 = 13000$ s (innermost contours). Panels B-D show the droplet footprints at simulation times $t_1 = 1900$ s (B), $t_2 = 8500$ s (C), and $t_3 = 13200$ s (D). The footprint diameters $L$ are plotted as function of time in (E); the evolution of $L$ cannot be analysed for $L < 0.1$ due to the diffuse interface nature of the numerical model. The times at which panels B-D are taken are indicated by the black arrows in panel (E).

section indicated by the dashed line in Fig. 5B. They illustrate how the middle droplet primarily responds to a concentration gradient in the vertical direction, whereas the droplets at the perimeter of the pattern also experience a gradient in the lateral directions. This should result in a reduced mass loss rate for the center droplet, as compared to the outer ones, and thus a relatively faster dissolution of the outer droplets. This is indeed the case, as shown by the droplet cross-sections (plotted at subsequent times $t_1 = 1900$ s, $t_2 = 8500$ s, and $t_3 = 13200$ s by the black dashed lines in Fig. 5A), by the top view images of the droplets (panels B-D), as well as by the evolution of the droplet footprint diameters in time (panel E). The cross sections in panel A also show that in the absence of pinning, the outer droplets dissolve asymmetrically, due to the higher mass loss rate at their exposed sides, i.e. fully
consistent with recent findings\textsuperscript{16}.

Comparable behavior is observed in experiments on patterns of droplets, as shown in Fig. 6. The droplets at the perimeter of the analyzed $n=23$ pattern dissolve more quickly than the inner droplets. The outermost droplets (numbers 5 and 6) disappear first, followed by the droplets placed in the middle row (numbers 2, 3, and 4). The dissolution time of the center droplet (number 1) is extended by $\approx 20\%$ as compared to an equally sized, single droplet. However, it is surprising to see that the dissolution times of the outermost droplets (5 and 6) are in fact much shorter ($\tau < 9100$ s) as compared to a single droplet. We interpret that this is most likely caused by the increased convection over this droplet pattern, caused by the larger amount of droplets, and hence the larger volume of (lighter) alcohol-saturated water. This stronger convection subjects the outermost droplets to an enhanced flow of clean water, increasing the dissolution rate and shortening the life time of the outermost droplets. Further inward in the pattern, the flow of water becomes progressively saturated by the dissolving droplets, reducing the dissolution rate from the innermost droplets and extending their dissolution time.

The initial footprints of the six droplets are indicated in red in panels A-C, illustrating that in contrast to the simulations, the droplet contact lines in the experiments are pinned by unavoidable local surface defects. This is especially visible for droplets 1 and 5, which are pinned to a point on their initial contact line throughout the entire dissolution process.

3.3 Droplet patterns: collective behavior
We now proceed by changing the number of droplets in the system and experimentally study the dissolution behavior in patterns of $n=5, 19, 41,$ and 127 droplets, placed at distances $d = 700 \mu m \pm 100 \mu m$ apart (see Fig. 1), such that $d/L_0 = 1.4 \pm 0.2$. The same spacing to diameter ratio is adopted in the simulations of pat-
To better appreciate the collective effect on the dissolution time, the experimentally and numerically measured dissolution times $\tau$ of the center droplets are plotted as function of $\log_{10}(n)$ in Fig. 8. The competition between the collective convective effect (increasing the dissolution rate and reducing the life time) and the collective diffusive effect (leading to an extended life time) is nicely visible in the experiments on small patterns ($n = 5, 19$): no significant increase of the life time as compared to a single droplet can be observed. In these small patterns, the effect of the convective flow is such that it counteract the shielding effect of the neighboring droplets. This shielding effect only becomes strong enough to counteract the effect of the collective convection in the larger patterns ($n = 41, 127$), where the dissolution time of the center droplet is extended significantly as compared to a single droplet ($\tau = 9100$ s). The effect of buoyancy driven convection is absent in the simulations, and hence a considerable increase of the droplet life time is already observed in the 5 droplet pattern.

### 3.4 Droplet patterns: effect of droplet spacing

So far, the droplets in all patterns, both in experiments and in numerics, were placed at a spacing to diameter ratio $d/L_0 = 1.4$. Still, for a given number of droplets in the experiments, the dissolution time of the center droplet is found to vary between experiments and we hypothesize that this is due to an unintentional variation in the positioning of the droplets, possibly resulting in $d/L_0 \neq 1.4$. To test the influence of the (relative) droplet spacing on the dissolution process, we maintain the same droplet size ($V_0 = 20 \text{ nL}, L_0 = 500 \mu\text{m}$), but construct patterns with different droplet spacing: the droplets were placed in a $n = 41$ pattern at ratios $d/L_0 = 1.1, 1.4, 2$, and 2.8 which we compared to simulations on infinite patterns with $d/L_0 = 1.5, 2.2, 5, 3$, and 5. Top boundary conditions were used in these simulations (Fig. 3, panel E3).

The resulting droplet volumes are plotted as function of time in Fig. 9, revealing that both in the experiments and in the simulations the dissolution time is considerably enhanced when the droplets are more densely packed. The dissolution time $\tau$ is plot-

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**Fig. 7** (color online) Volume of the center droplet as function of time, as obtained from experiments (A) and numerics (B), for individual dissolving droplets and droplet patterns of various sizes. Volume and time in panel A have been rescaled (as described in section 3.1, see Eqs. (3) and (6)) to correct for small differences in the initial droplet volumes. Lines in (A) represent the mean of multiple experiments. The error bars indicate the spreading between different repetitions of the experiment.
ted as function of $d/L_0$ in Fig. 10 for both the experiments and simulations for direct comparison. It should be noted that in the limit $d/L_0 \to \infty$ (i.e., a single droplet), the simulations are not expected to result into the same behavior as the single droplet treated in section 3.1, due to the different boundary conditions used.

Our simulations confirmed the earlier hypothesis\(^4\) that the reduced dissolution rate is caused by an increased concentration in between the droplets, lowering the concentration gradient and thus the dissolution rate. This effect was weaker at the edge of the pattern, causing the outermost droplets to dissolve more quickly than the inner droplets, an effect found in both the simulations and experiments.

Future numerical work should incorporate the effect of natural convection, or future experimental work could eliminate convection, for example by reducing droplet sizes, or conducting the dissolution experiments in a micro-gravity environment\(^17\). Also, the current experimental system was limited by the fact that it could only measure the center droplet of the pattern. Future work could be improved by simultaneous volumetric measurements of all droplets in the pattern, for example through top view imaging combined with interferometry to obtain height profiles of the dissolving droplets\(^18\).

### Acknowledgments

Andrea Prosperetti and Xuehua Zhang are gratefully acknowledged for continuing inspiring discussions. Maaike Rump and Kevin Hofhuis are acknowledged for assistance during the experiments.
Appendix: Numerical model

We describe the binary fluid by the Cahn-Hilliard free energy\(^\text{19,20}\)

\[
\mathcal{F} = \int (\mathcal{F}_b + \frac{\kappa}{2} |\nabla \phi|^2) \, dV + \int g(\phi) \, dS
\]  \hspace{1cm} (7)

where

\[
\mathcal{F}_b = \frac{\rho}{3} \log \rho + \frac{a}{2} \phi^2 + \frac{b}{4} \phi^4
\]  \hspace{1cm} (8)

is the bulk free energy. The first term in the bulk free energy is an ideal gas term, \(\rho\) the density field and \(a\) and \(b\) model parameters. With this choice of the free energy, phase separation occurs if \(a < 0\) and \(b > 0\) and the \(\phi\) field in each phase takes the values \(\phi^\pm = \pm \sqrt{-a/b}\). The second term in Eq. (7) represents the surface tension, which takes the value \(\gamma = \sqrt{-8ka^3/9b^2}\). This is a diffuse interface model and the interface width is \(\sqrt{2\kappa/\alpha}\).

In the limit of negligible convection the concentration field evolves following to the diffusion equation

\[
\frac{\partial \phi}{\partial t} = M\nabla^2 \mu.
\]  \hspace{1cm} (9)

where \(M\) is the mobility and the chemical potential

\[
\mu = \frac{\delta \mathcal{F}}{\delta \phi} = a\phi + b\phi^3 - \kappa\nabla^2 \phi.
\]  \hspace{1cm} (10)

We solve Eq (9) using a Lattice-Boltzmann algorithm. Details are given in ref.\(^\text{21}\). The parameters are \(-a = b = 0.00305\), \(\kappa = 0.0078\) and \(M = 5\) and \(\rho = 1\). The simulation domain was of size \((N_x, N_y, N_z) = (100, 100, 50)\) for the single drop and infinite pattern case, and \((N_x, N_y, N_z) = (200, 200, 50)\) for the five droplet pattern. Unless stated otherwise, the initial footprint diameter of the drop was \(L_0 = 60\). This choice of parameters has already been validated in\(^\text{12}\).

The chemical potential is fixed at the boundaries as described in section 2.2 by fixing the order parameter \(\phi\) and using Eq. 10. Details are given in ref.\(^\text{12}\).

References