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2	pathways in Methanosarcina barkeri
3	
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1 Abstract

2 Ammonia is a ubiquitous potential inhibitor of anaerobic digestion processes, mainly exhibiting inhibition towards methanogenic activity. However, knowledge as to how 3 ammonia affects the methanogens is still limited. In this study, we cultured a 4 multitrophic methanogen, Methanosarcina barkeri DSM 800, with acetate, H₂/CO₂, 5 and methanol to evaluate the influence of ammonia on different methanogenic 6 pathways. Aceticlastic methanogenesis was more sensitive to increased ammonia 7 concentrations than hydrogenotrophic and methylotrophic methanogenesis. Theoretical 8 9 maximum NH₃ tolerances of *M. barkeri* fed with acetate, H₂/CO₂, and methanol were 10 calculated to be 39.1 ± 9.0 , 104.3 ± 7.4 , and 85.7 ± 1.0 mg/L, respectively. The order of the ΔG range of *M. barkeri* under three methanogenic pathways reflected the order 11 12 of ammonia tolerance of *M. barkeri*. Our results provide insights into the role of the thermodynamic potential of methanogenesis on the tolerance of ammonia stress; and 13 shed light on the mechanism of ammonia inhibition on anaerobic digestion. 14

15

16 Keywords: Ammonia tolerance, *Methanosarcina barkeri*, Gibbs free energy,
17 Thermodynamic restriction

18 **1 Introduction**

19 Methanogenic degradation of organic waste to methane and carbon dioxide is a common biochemical process performed by the cooperation of bacteria and 20 21 methanogens in oxygen-limited environments, and increasingly applied as an effective 22 and environmentally friendly technology for energy recovery from the recycling of organic waste (Demirel et al. 2008). In anaerobic digestion (AD), the final 23 24 methanogenic pathways are normally divided into three categories according to their 25 substrate utilization spectrum: CO₂ reducing (hydrogenotrophic), acetate splitting (aceticlastic) and methyl reducing (methylotrophic) pathway(Angel et al. 2011). In 26 27 addition, two novel pathways capable of methanogenic degradation of methoxylated aromatic compounds (Mayumi et al. 2016) and long-chain alkanes (Zhou et al. 2022) 28 29 have recently been reported, however, these pathways are always restricted to natural and subsurface environment. 30

31 Ammonia is a common inhibitor in AD, especially in reactors treating protein-rich 32 substrates (Rajagopal et al. 2013), and mainly inhibits the methanogenic activity (Calli 33 et al. 2005, Duan et al. 2022). Excessive ammonia results in an increase in lag-phase and a decrease of methanogen growth rate and methane production (Hansen et al. 1998, 34 35 Yu et al. 2020). In most reported cases of AD, aceticlastic methanogens were observed 36 to be much more sensitive than hydrogenotrophic methanogens under ammonia stress 37 (Lue et al. 2013, Ruiz-Sánchez et al. 2017, Lv et al. 2019). The un-ionized ammonia (NH₃), rather than ionized ammonium is considered the more toxic species (Tian et al. 38

39	2018a, Astals et al. 2018). Mechanisms proposed to explain ammonia inhibition of
40	methanogens include efflux of intracellular K^+ (Sprott et al. 1984, 1985, 1986) and
41	inhibition of genes related to methanogenic metabolism (Duan et al. 2022, Kato et al.
42	2014, Kato et al. 2008, Zhang et al. 2018, Zhang et al. 2014, Yan et al. 2020). However,
43	these generic mechanisms cannot explain the observed variation of ammonia tolerance
44	of diverse methanogenic pathways in the methanogenic consortia (Lue et al. 2013,
45	Ruiz-Sánchez et al. 2017, Lv et al. 2019). In order to unlock the black box of ammonia
46	inhibition in AD, it is necessary to further research the flexible response of different
47	methanogenic pathways to ammonia.
48	In this study, we cultivated a multitrophic methanogen, <i>M. barkeri</i> strain DSM 800

48 In this study, we cultivated a multitrophic methanogen, *M. barkeri* strain DSM 800, 49 with acetate, H_2/CO_2 or methanol as sole carbon and energy source, respectively. Based 50 on physiological profiles, transcriptomic analyses and thermodynamic calculations, the 51 ammonia tolerance of three methanogenic pathways of *M. barkeri* was compared. This 52 comparison gave an in depth understanding of the mechanism of ammonia inhibition 53 in methanogenesis.

54 2 Materials and methods

55 2.1 Cultures and growth conditions

Methanosarcina barkeri DSM 800 was obtained from the China Collection of
Anaerobic Microorganisms (CCAM). *M. barkeri* was grown using a medium with the
following composition (in g/L): K₂HPO₄, 0.35; KH₂PO₄, 0.23; NH₄Cl, 1.0; MgSO₄,
0.25; NaCl, 2.25; yeast extract, 2.0; cysteine-HCl·H₂O, 0.5; Na₂S·9H₂O, 0.25; trace

60 element solution SL-10, 1 mL (Chin et al. 1998); vitamin solution, 1 mL (Wolin et al. 1963); 0.1% (w/v) resazurin solution, 1 mL. M. barkeri was incubated in 650-mL sealed 61 nitrogen-filled serum bottles with a 270-mL medium volume. These serum bottles were 62 divided into several treatments according to carbon source and the concentration of 63 64 ammonia (Table S1). The culture bottles were inoculated with 30 mL of inoculum 65 cultivated with the corresponding carbon source and headspaces were filled with N₂. 66 The initial pH values of all treatments were controlled at 7.0 ± 0.1 and MOPS buffer (final concentration of 50 mM) was added as a pH buffer. Triplicate and quintuplicate 67 68 incubations were conducted for blank treatment and treatment with added substrate, respectively, and incubated at 37 °C with shaking (100 rpm). 69

70 2.2 Chemical analysis

71 CO₂ and CH₄ in gas samples were determined by gas chromatography (Agilent 72 7820A, USA) (Zhou et al. 2022). H₂ was analyzed by gas chromatography (Pu Chuang GC 6800T, China) (Jiao et al. 2021). Acetate and methanol were measured by high-73 74 performance liquid chromatography (Agilent HPLC 1200, USA) (Cheng et al. 2013). 75 Gas pressure and pH were measured by pressure gauge (Ashcroft 2084, USA) and pH meter (Horiba B-712, Japan), respectively (Zhou et al. 2022). Total ammonia 76 77 concentration was quantified by Nessler's reagent colorimetric method following the 78 standard methods (Greenberg et al. 1992).

79 2.3 RNA extraction and transcriptomic analysis

Samples from the control treatments (0.5 g/L NH₄Cl) and treatments with high 80 NH₄Cl concentration (10 g/L NH₄Cl for acetate, 20 g/L NH₄Cl for H₂/CO₂ and 81 methanol) at multiple time points over the logarithmic period were selected for 82 83 transcriptomic analysis. Triplicates in each treatment were used for RNA transcripts. 84 RNA was extracted using RNAprep pure Cell/Bacteria Kit (Cat. No. DP430; TIANGEN, Beijing, China). The genome of M. barkeri DSM 800 (RefSeq: 85 86 GCF 000970025.1) was downloaded from National Center for Biotechnology 87 Information (NCBI, https://www.ncbi.nlm.nih.gov/). Quality trimming of the transcriptomic sequences was performed by Trimmomatic v0.36 and mapped to CDS 88 89 (coding sequence) using the BWA (http://bio-bwa.sourceforge.net). RNA expression was calculated by transcripts per kilobase of exon model per million mapped reads 90 91 (TPM) (Wagner et al. 2012).

92 2.4 Statistical analyses

The ammonia effect on the general changes of gene expression was assessed by principal component analysis (PCA) in R (<u>http://www.r-project.org/</u>), using the vegan package (Mendes et al. 2008). The t-test was used to determine whether the individual gene expression varies in the different treatments (Only differences between treatments with the same carbon source but different ammonia concentrations for the same period were shown). The absolute value of log₂foldchange >1 and p value <0.05 were used to identify differentially expressed genes (DEGs). To reflect the similarities and

103	2.5 Calculations
102	software (packages: psych (Revelle 2008)).
101	(Mamakani et al. 2012) in R was used. Pearson correlation test was performed using R
100	differences in DEGs in the different carbon source treatments, the Venn package

104 The moles of
$$H_{2}$$
, CH_{4} and CO_{2} were calculated from the equilibrium of Eq. (1).

104

107

105
$$n_i = P_i * V/R * T$$
 (1)

106 Where n_i is mole of i, P_i is partial pressure of i V is the volume over the bottle, R is the universal gas constant (8.314 J/K·mol) and T is the temperature in Kelvin.

Free ammonia concentrations were calculated from the equilibrium of Eq. (2) as 108 described previously (Calli. et al. 2005). 109

110
$$[NH_{3}] = \frac{[TNH_{3}]}{1+10^{\left(0.09018 + \frac{2729.92}{T(K)} - pH\right)}}$$
(2)

111 where [NH₃] is the free ammonia concentration, [TNH₃] is the total ammonia concentration and T(K) is the kelvin temperature. 112

The maximum specific methane production rate (μ_{max}) of *M. barkeri* DSM 800 113 was calculated from methane accumulation curve in the logarithmic period as described 114 in detail by Zhou ((Zhou et al. 2022). 115

For the thermodynamic calculations, the reactions evaluated were as follows: 116

117
$$CH_3COO + H^+ \rightarrow CH_4 + CO_2, 4H_2 + CO_2 \rightarrow CH_4 + 2H_2O, 4CH_3OH \rightarrow 3CH_4 + CO_2 + 2H_2O,$$

118 For a reaction
$$aA + bB \rightarrow cC + dD$$
, ΔG was calculated from the equilibrium of

Eq. (3) as described previously (Dolfing 2015). 119

120
$$\Delta G = \Delta G^{\theta} + RT \ln \{ [(C)c(D)d]/[(A)a(B)b]$$
(3)

Where ΔG^{θ} values were taken from Amend and Shock (Amend 2001), R is the 121 universal gas constant (8.314 J/K·mol) and T is the temperature in Kelvin. 122

123 **3 Results**

124 3.1 Effects of ammonia on the growth of *M. barkeri*

125 Incubation of *M. barkeri* with acetate, methanol, and H₂/CO₂ respectively, was performed under different NH₄Cl conditions. The physiological response of *M. barkeri* 126 127 to NH₄Cl stress was dramatically different under three methanogenic carbon source 128 conditions (Fig. 1, Table 1). No methane was detected in 15, 40 and 30 g/L NH₄Cl groups for the acetate, methanol, and H₂/CO₂ treatment, respectively (Fig. 1, Table 1). 129 The lag period increased from 2 to 26 days for acetate treatment when the concentration 130 131 of NH₄Cl was increased from 0.5 to 10 g/L (Fig. 1a, Table 1). However, the delay was only 3 days and 1 day for methanol and H₂/CO₂ treatments when NH₄Cl increased to 132 133 20 and 30 g/L, respectively (Fig. 1a, Table 1).

134 pH in three substrate treatments fluctuated, within an average range of 0.3 units in the methane production period (Fig. S1). For the total ammonia concentration remained 135 essentially constant (Fig. S2), the NH₃ of different substrates calculated based on Eq. 136 (1) (Calli. et al. 2005) varies slightly(Fig. S2). The μ_{max} decreased with increasing NH₃ 137 concentration under all three substrate treatments (Fig. 2, Table 1), and exhibited a 138 negative linear correlation with NH₃ concentration ($R^2 > 0.96$) (Fig. 2a, Table 2). Based 139 on these regression equations, the theoretical maximum NH₃ tolerance for acetate, 140 methanol, and H₂/CO₂ utilization were calculated to 39.1 ± 9.0 , 104.3 ± 7.4 , and 85.7141

142 \pm 1.0 mg/L (i.e., the NH₃ concentration where $\mu_{max} = 0$), respectively (Fig. 2a). The 143 maximum ammonia tolerance of *M. barkeri* from methanogenic precursors was 144 H₂/CO₂ > methanol > acetate, which indicated the aceticlastic methanogenic pathway 145 was much more sensitive than hydrogenotrophic and methylotrophic methanogenic 146 pathways.

147 The ΔG values calculated during the methane accumulation stage gradually increased from -65 to -30 kJ/reaction for aceticlastic methanogenesis, from -108 to 148 -73 kJ/reaction for methylotrophic methanogenesis, and from -136 to -90 kJ/reaction 149 for hydrogenotrophic methanogenesis respectively (Fig. S3a). Standard Gibbs free 150 energies are -80, -107, and -126 kJ/mol for acetate, methanol and H₂/CO₂, respectively 151 (Table S2). The order of the ΔG range of *M. barkeri* under three methanogenic 152 153 pathways was in agreement with the ammonia tolerance of *M. barkeri*, i.e., $H_2/CO_2 >$ methanol > acetate. Noteworthy, a positive linear relationship between the theoretical 154 maximum NH₃ tolerance for different substrates and their ΔG was observed. These 155 trends remained stable under different incubation time ranged from the initial time point 156 (t₀), to the half concentration of substrate consumed (t₅₀), or standard conditions ($R^2 >$ 157 0.99) (Fig. 2b). 158

159 **3.2 Transcriptomic analysis**

PCA analysis results showed gene expression of different samples with the same
substrate and ammonia concentration at different sampling periods was clustered (Fig.
S4), indicating that the substrate and ammonia had significant impact on the gene

expression of *M. barkeri*. For treatments of acetate, methanol and H₂/CO₂, there were
516-546, 535-445, and 311-348 down-regulated genes and 471-398, 446-522, and 290372 upregulated genes in response to high ammonia stress at the two sampling time
points, respectively (Fig. S5 and S6). *M. barkeri* were more significantly affected by
ammonia when using acetate and methanol than when using H₂/CO₂.

168 The genes involved in individual methanogenic pathways were not specifically 169 down-regulated. Down-regulation of genes was essentially consistent between acetate and methanol treatments, including all subunits of tetrahydromethanopterin S-170 methyltransferase (*mtr*), heterodisulfide reductase subunit E (*hdr*E), and most of the 171 172 subunits of V-type ATP synthase (*atp*) (Fig. 3). Sodium/proton antiporter (*nha*) was observed to be significantly down-regulated in both H₂/CO₂ and methanol groups (Fig. 173 174 3). In H₂/CO₂ treatment *atp* and *mtr* were no statistically but differentially downregulated (Fig. 3). In general, inhibition of methanogenic pathways by ammonia was 175 176 general rather than selective.

Previous studies have reported that ammonia stress causes efflux of intracellular 177 K^+ (Sprott et al. 1985, 1984, 1986). Therefore, we further investigated the expression 178 of genes involved in the K^+ transport systems. Trk system K^+ uptake protein (*trk*) and 179 180 glutathione-regulated K^+ -efflux system ancillary protein (*kefG*) were up-regulated in the presence of high ammonia in acetate treatment (Fig. 4). In methanol treatment, the 181 up-regulated genes were K^+ -efflux system ancillary protein (*kefG*), K^+ channel protein 182 (kch), and large conductance mechanosensitive channel (mscL) (Fig. 4). No 183 significantly regulated gene responsible for K^+ transport was observed in H₂/CO₂ 184

treatment (Fig. 4). According to transcriptomic results, the degree of K⁺ efflux caused
by ammonia was different in different treatments.

187 **4 Discussion**

188 We observed that the impact of ammonia stress on methanogenic activity was directly related to the active methanogenic pathway, which could not be explained by 189 the hypotheses previously put forward in the literature, such as K⁺ flux and selective 190 inhibition of the expression of key genes involved in methanogenesis (Yu et al. 2020, 191 192 Sprott et al. 1986, Kato et al. 2014, Wang et al. 2015). Sprott et al. (1986) proposed ammonia induced efflux of the cytoplasmic K^+ through an ammonia/ K^+ exchange 193 194 reaction. The higher the concentration of ammonia, the larger the K⁺ loss, and the more severely the cells are inhibited. However, the effects of the same methanogen grown 195 196 under different methanogenic pathways were significantly different, the differential response could not be fully explained by the hypothesis of K^+ loss, which has also 197 been argued by Hendriksen et al. (1991). 198

Functional genes involved in different methanogenic pathways were possibly specifically inhibited (Yu et al. 2020, Kato et al. 2014). However, our transcriptomic analysis showed that ammonia repressed the expression of genes involved in different methanogenic pathways in a general rather than a specific way. The relevant genes involved in only a single methanogenic pathway were not significantly down-regulation under ammonia stress. Instead, genes *mtr*, *nha* and *atp* involved in energy metabolism of all three pathways simultaneously were significantly regulated by ammonia (Fig. 3), others studies have found those genes down-regulated in response to high ammonia
stress by transcriptomic analysis (Kato et al. 2010, Yan et al. 2020, Xing et al. 2021,
Kato et al. 2014). A decrease in ATP content was also observed as ammonia
concentration increased (Wang et al. 2022).

Taking the above findings into account, the previous hypotheses to explain the 210 211 difference in ammonia tolerance of different methanogenic pathways had some 212 drawbacks. It was reported that variable capabilities of ammonia tolerance might depend on the difference in ΔG of reactions with different substrates (Yan et al. 2020), 213 and higher energy metabolism level might be conducive to counteract ammonia stress 214 215 (Wang et al. 2022). However, these findings could not exclude influence of other microorganisms because these results were obtained from complex microflora. We 216 217 cultivated a multitrophic methanogen with three methanogenic pathways to circumvent this effect and demonstrated more clearly, that the toxicity of NH₃ was related to ΔG of 218 219 methanogenesis with corresponding precursors. ΔG is a thermodynamic potential and the maximum amount of energy available from one chemical reaction (Zhang and 220 Reece 2019), which is conserved in the form of reducing power and ATP in 221 methanogens. The reducing power decreased because the intracellular NH₃ competed 222 223 for protons with endoenzymes that catalyzed the production of reducing power (Yu et al. 2021). The latter was consumed when the cells counteracted the presence/damage 224 225 of NH₃ (Yan et al. 2020). Consequently, less energy was produced and more was consumed, causing an energy drain. Methanogenic processes that produce more energy 226 227 will consequently be more resistant to ammonia stress. On the other hand, the same

energy was required for cell maintenance in same cell, however, the energy produced
by cells cultured with different substrates was different. Which meant that the ratio of
energy flux between maintenance and production was different for each substrate. The
cells with a higher relative maintenance energy contribution were more sensitive to
ammonia and stopped growing at a lower ammonia concentration.

233 Our findings demonstrate that, due to the influence of thermodynamic limitation, 234 the ranking of ammonia tolerance of the typical three methanogenic pathways of M. *barkeri* is hydrogenotrophic > methylotrophic > aceticlastic. Similar results were found 235 at the community level despite the variability of species and methanogenic pathways. 236 237 A number of studies found that the ammonia tolerance of hydrogenotrophic and methylotrophic methanogens was higher than that of aceticlastic methanogens in 238 239 complex microbial community systems (Lue et al. 2013, Ruiz-Sánchez et al. 2017, Lv et al. 2019, Yan et al. 2020, Fujishima et al. 2000, Chen et al. 2016, Tian et al. 2018b, 240 241 Sun et al. 2021). Kato et al. (2014) evaluated the inhibitory effects of ammonia on two different degradation pathways using a pure culture (aceticlastic methanogen) and 242 defined co-culture (hydrogenotrophic methanogen and syntrophic acetate-oxidizing 243 bacteria), the results demonstrated that aceticlastic methanogen was sensitive to 244 245 ammonia stress than hydrogenotrophic methanogen. Although the resistance of acetate-246 consuming methanogens to high ammonia stress has also been reported, however these aceticlastic methanogens reported were Methanosarcina (Fotidis et al. 2013, Hao et al. 247 2015), which are a multitrophic methanogens. Indeed, there are indications that 248 Methanosarcina may act as hydrogen-utilizing methanogen in microbial communities 249

under ammonia stress (Westerholm et al. 2012), which suggests that under duress *Methanosarcina* may shift to the thermodynamically best option. The multiple
methanogenic metabolisms of *Methanosarcina* confers adaptability and contributes to
its adaptation to environmental stress.

254 5 Conclusions

255 This study revealed that the ranking (highest to lowest) of ammonia tolerance of methanogenic pathways is hydrogenotrophic > methylotrophic > aceticlastic. And our 256 results clearly showed the relationship between thermodynamic potential and ammonia 257 tolerance, revealing the ammonia tolerance of *M. barkeri* was determined by 258 259 thermodynamic restriction. The study provides a theoretical basis for a relative ammonia inhibition tolerance for H₂ vs acetate. These findings advance understanding 260 261 of how ammonia inhibits methanogens, extending and refining the model of ammonia inhibition in methanogens. Further physiological and molecular biological experiments 262 are needed to comprehensively understand ammonia inhibition in methanogenic 263 ecosystems and beyond. 264

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271 Data Availability Statement

272 The raw reads of the transcriptomics sequencing are available at the NODE

database (<u>https://www.biosino.org/node/</u>) by accession number OEP003314.

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Fig. 1 Methane production and substrate consumption in treatments supplemented with different substrates and different ammonia concentration. (a and d) Acetate treatment; (b and e) H_2/CO_2 treatment; (c and f) Methanol treatment. The dashed line is the theoretical methane production when the substrate is completely consumed.

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Fig. 2 Relationship between NH_3 -N concentration and maximum specific methane production rate (a) and relationship between standard Gibbs free energy and theoretical maximum NH_3 tolerance (b). t₀: Initial time point, t₅₀: Time where 50% of the substrate has been consumed. The CH_4 and CO_2 concentrations at t₀ were assumed to be 0.1%.

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Fig. 3 Metabolic pathway and heatmap of log_2 foldchange for key genes involved in methanogenesis of *M. barkeri* under ammonia stress. * : To avoid duplication, this gene was only shown in the first heatmap. Genes involved in different pathways was colour coded as follows: green (hydrogenotrophic), red (aceticlastic), blue (methylotrophic), yellow (hydrogenotrophic and aceticlastic), orange (hydrogenotrophic and methylotrophic), and blank (all pathway). a: methanogenic pathway, b: energy conservation.



Fig. 4 Heatmap of log_2 foldchange for gene involved in K⁺ transport system of M.

barkeri under ammonia stress.

Carbon source	added M (g/L)	NH ₄ C	^l Detected NH ₄ ⁺ - N (mg/L)*	Calculated NH ₃ -N (mg/L)*	Lag period (d)	Maximum methane pro rate (/d)	specific duction	
Acetate	AC0.5	0.5		NT	NT	NT	NT	
Acetate	AA0.5	0.5		262.6 ± 8.1	3.0 ± 0.2	<2	0.21 ± 0.01	
Acetate	AA5	5		1126.5 ± 65.7	13.4 ± 1.5	<8	0.19 ± 0.01	
Acetate	AA10	10		2391.5 ± 61.9	26.3 ± 1.4	<26	0.07 ± 0.01	
Acetate	AA15	15		NT	NT	NT	NT	
H_2/CO_2	HC0.5	0.5		NT	NT	NT	NT	
H ₂ /CO ₂	HH0.5	0.5		271.1 ± 2.9	2.2 ± 0.3	<2	0.19 ± 0.01	
H ₂ /CO ₂	HH10	10		2776.8 ± 37.4	24.1 ± 2.8	<2	0.16 ± 0.02	
H_2/CO_2	HH20	20		5320.1 ± 68	42.7 ± 5.1	<3	0.12 ± 0.01	
H_2/CO_2	HH30	30		7204.5 ± 162.1	58.7 ± 7.6	<3	0.08 ± 0.01	
H_2/CO_2	HH40	40		NT	NT	NT	NT	
Methanol	MC0.5	0.5		NT	NT	NT	NT	
Methanol	MM0.5	0.5		278.5 ± 6.9	3.8 ± 0.2	<3	0.62 ± 0.03	
Methanol	MM10	10		2559.2 ± 42	31.6 ± 4.5	<5	0.48 ± 0.02	
Methanol	MM20	20		4935.5 ± 48.4	54.6 ± 0.3	<6	0.23 ± 0.01	
Methanol	MM40	40		NT	NT	NT	NT	

Table 1 Ammonia concentration and growth properties of M. barkeri DSM 800

* : Initial concentration of NH₃-N, NT: Not tested

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Highlights

- 1. Differential ammonia tolerance of *M. barkeri* was observed under three different methanogenic pathways.
- 2. The Maximum NH₃ tolerances of *M. barkeri* fed with acetate, H_2/CO_2 , and methanol were 39.1 ±

9.0, 104.3 \pm 7.4, and 85.7 \pm 1.0 mg/L, respectively.

3. Thermodynamic restrictions were the key factor determining the ammonia tolerance of the three

methanogenic pathways.